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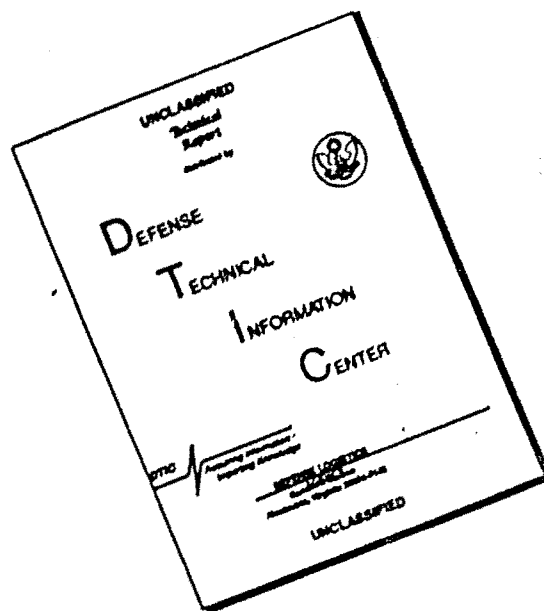
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# HEAT TRANSFER EFFECTS ARISING FROM ARC ROTATION IN PLASMA ARC HEATERS OF THE SELF-INDUCED MAGNETIC FIELD TYPE

by E. A. BUNT

THE JOHNS HOPKINS UNIVERSITY • APPLIED PHYSICS LABORATORY

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## SUMMARY

This paper is concerned with an analysis of the thermal behavior of high input power ( $\sim 15$  Megawatt) arc heaters operating at values of total (bulk) enthalpy up to 2500 Btu/lb. Such heaters are currently in use to supply air for aerodynamic testing purposes, including subsonic turbulent pipe flow, the operation of propulsion tunnels with "full" temperature simulation, and supersonic combustion ducts. The electrode system is essentially a "rail accelerator" adapted for continuous operation by making it re-entrant; the self-induced magnetic field brings about rapid movement of the arc roots to prevent destruction of the electrodes. The rate of rotation of the arc column (which is subject to aerodynamic drag) is shown to be a function of apparent electrode gap and current and the stagnation temperature and pressure in the arc chamber. A distinction can also be drawn between "long" and "short" arcs, depending on whether the interelectrode gap is large or small. The value of the arc rotation rate,  $\omega$  (which ranges between approximately 50 and  $1000 \text{ sec}^{-1}$ ) had a considerable bearing on the thermal efficiency of short-gap arcs because of the dependence of the convective losses on it. Since the chamber gases radiated much more strongly than air uncontaminated by electrode material, convective and radiative losses are distinguished by solving for first-power and fourth-power dependence on temperature difference with the walls; the convective losses are examined in conjunction with a vortex model of the gas behavior.

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## 1. INTRODUCTION

This paper is concerned with the heat losses occurring in high-power ( $\sim 15$  Megawatt input), electrothermal (plasma arc) heaters which operate at bulk enthalpies up to 2500 Btu/lb. The production of dense plasmas is of considerable importance in the simulation of high velocity flight; three such heaters are presently in use at The Johns Hopkins University Applied Physics Laboratory to supply air at temperatures up to about 7000°R for such purposes as the operation of full-temperature simulation hypersonic tunnels, supersonic combustion ducts, and tunnels for testing re-entry ablation materials (Ref. 1). These heaters make use of a split-electrode system that generates a self-induced magnetic field for the purpose of rapidly moving the arc around the electrodes, thereby eliminating the need for an external field coil. This approach was dictated by the characteristics of the available power supply, a large submarine battery (Ref. 1), that favor the use of large currents but not of high voltages.

Of the three main heat loss mechanisms, arc radiation, gas radiation, and convection, the last two were believed to be predominant because of the wide variation of overall efficiency, depending on the choice of operating variables. Any continuously rotating arc generates a strong vortex, and the efficiency was found to be a function of the arc rotation rate (which varied between 50 and 1000  $\text{sec}^{-1}$ , depending mainly on current and pressure). It was important to know the relative proportions of forced convection and radiation losses at moderate enthalpies to provide

a rational basis for reducing convective losses to a minimum and to obtain information on gas emissivities that would be useful in indicating what limit would be placed on chamber size when much higher enthalpy running was undertaken, since it was suspected that calculations based on pure air radiation tables would be inapplicable.

In this paper, the electrode operation is first described. The relationship between arc rotation and current, pressure, and electrode gap is then investigated for a split-ring arc. The measurement of arc rotational velocity having been dealt with, the effects of the vortex and the chamber geometry on heat transfer are then discussed, and a model is advanced to account for the observed effects.



## 2. NOTATION (Excluding Constants)

a	Distance between center lines of electrodes, ft
A	Area, $\text{ft}^2$
b	Width of arc chamber, ft
B	Field strength, lines $\text{cm}^{-2}$
$C_d$	Drag coefficient, dimensionless; discharge coefficient, dimensionless
$c_p$	Heat capacity at constant pressure, $\text{Btu}(\text{°R})^{-1} \text{ slug}^{-1}$
d	Diameter of arc chamber, ft; length parameter in Reynolds and Nusselt numbers, ft; diameter of arc column, cm
$f(\ell)$	Arc gap function ( $= 2 \ln [(\ell+R)]$ ), dimensionless (see Eq. (1))
$f(q)_n$	Geometrical function ( $= x^c$ ), $\text{Btu ft}^{1.6} \text{ sec}^{-1} (\text{°R})^{-1}$ (see Eqs. (5-9))
$f^c(T)$	Convective function ( $= (T_g - T_w)(\omega/\nu)^{0.8}$ , $(\text{°R}) \text{ ft}^{-1.6}$ )
$f^r(T)$	Radiative function ( $= T_g^4$ ), $(\text{°R})^4$
h	Film coefficient, $\text{Btu ft}^{-2} \text{ sec}^{-1} (\text{°R})^{-1}$
H	Enthalpy, $\text{Btu lbm}^{-1}$
I	Discharge current, amps; radiation intensity per unit volume, $\text{Btu ft}^{-3} \text{ sec}^{-1}$
k	Thermal conductivity, $\text{Btu ft}^{-1} \text{ sec}^{-1} (\text{°R})^{-1}$
L	Length, ft
$\ell$	Interelectrode gap, ft (unless otherwise stated) Effective length of arc track, ft
$\dot{m}$	Mass flow, $\text{lbm sec}^{-1}$

Nu	Nusselt number ( $= hd/k$ ), dimensionless
p	Electrode perimeter, ft
P	Pressure, psia (unless otherwise stated); heat power, Btu sec <sup>-1</sup>
Pr	Prandtl number ( $= c_p \mu/k$ ), dimensionless
$\dot{q}$	Heat flux, Btu sec <sup>-1</sup>
r	Radial distance, cm or ft
R	Gas constant ( $= 1716$ ), ft <sup>2</sup> sec <sup>-2</sup> (°R) <sup>-1</sup> ; cross-sectional radius of electrode, ft
Re	Reynolds number ( $= dvp/\mu$ ), dimensionless
St	Stanton number $h/V\rho c_p \mu$ , dimensionless
T	Temperature, °R
v	Discharge voltage, volts
V	Volume of arc chamber, ft <sup>3</sup> ; velocity, ft sec <sup>-1</sup>
$x_n^c$	Geometrical function ( $= f(\dot{q})_n$ ), Btu ft <sup>1.6</sup> sec <sup>-1</sup> (°R) <sup>-1</sup>
$x_n^r$	Geometrical function ( $= 2\sigma V(\epsilon/L)A_n/A_{total}$ ), Btu sec <sup>-1</sup> (°R) <sup>-4</sup>
Z	Compressibility factor, dimensionless
$\gamma$	Ratio of specific heats, dimensionless
$\epsilon/L$	Emissivity per unit thickness, ft <sup>-1</sup>
$\eta$	Overall efficiency (fractional)
$\mu$	Dynamic viscosity, slug ft <sup>-1</sup> sec <sup>-1</sup>
$\nu$	Kinematic viscosity, ft <sup>2</sup> sec <sup>-1</sup>
$\rho$	Mass density, slug/ft <sup>3</sup>
$\sigma$	Boltzmann's constant ( $= 4.81 \times 10^{-13}$ ), Btu ft <sup>-2</sup> sec <sup>-1</sup> (°R) <sup>-4</sup>
$\omega$	Arc rotation rate, sec <sup>-1</sup>

### Subscripts

c	Convective
cyl	Cylindrical section
elec	Electrode
end	End plate
forced	Forced vortex
g	Gas
h	Hydraulic
i	Cooling channel designation
induced	Induced vortex
m	Metering; run designation
n	Surface exposed to heating
p	Constant pressure
r	Radiative
t	Stagnation
w	Wall
o	Standard electrode gap (= 0.141 ft)
1	Radius of arc chamber exit duct
2	Radius of equivalent circular arc path
3	Outer radius of arc chamber

### Superscripts

*	Sonic value
'	Unheated condition

A bar (  $\bar{\phantom{x}}$  ) indicates a mean value

### 3. EXPERIMENTAL APPARATUS AND MEASUREMENTS

3.1 Arc Operation and Overall Design--The design of an arc unit has much in common with that of a magnetohydrodynamic duct. The essence of the design used here is the use of the rail accelerator (Refs. 2-4) electrode system, which has been adapted for continuous DC operation by making it re-entrant; this principle has now been in use for some years in arc heaters in various laboratories, both with three-phase AC (Refs. 5-7) (three or four electrode types) and with DC (Refs. 8-13) (two electrode types) power supplies. Operational experience in the latter mode--which is the more satisfactory of the two--has been gained over the range of current values  $8 < I < 32$  kamps. Figure 1 shows a cut-away view of the unit, the details of many of the components of which are similar to those of a steel arc described in Ref. 9. The pressure vessel or heat exchanger, in which the arc rotated, was made of forged chrome copper to combine sufficient strength with high thermal conductivity for cooling purposes; it consisted basically of a cylindrical section of internal diameter 19.75 inches closed by two end plates spaced 11 inches apart. These three sections were in electrical contact, but the unit as a whole was electrically floating since the power supply to the electrodes was grounded during discharge. Cooling channels were also machined within all the main components of the pressure vessel. Since welding of such large copper masses was not feasible, copper tapered plugs were driven into all holes that required closing.

The air flow system was a "hard" one, i. e., the pressure chamber was located between two sonic orifices. The first orifice was used for flow

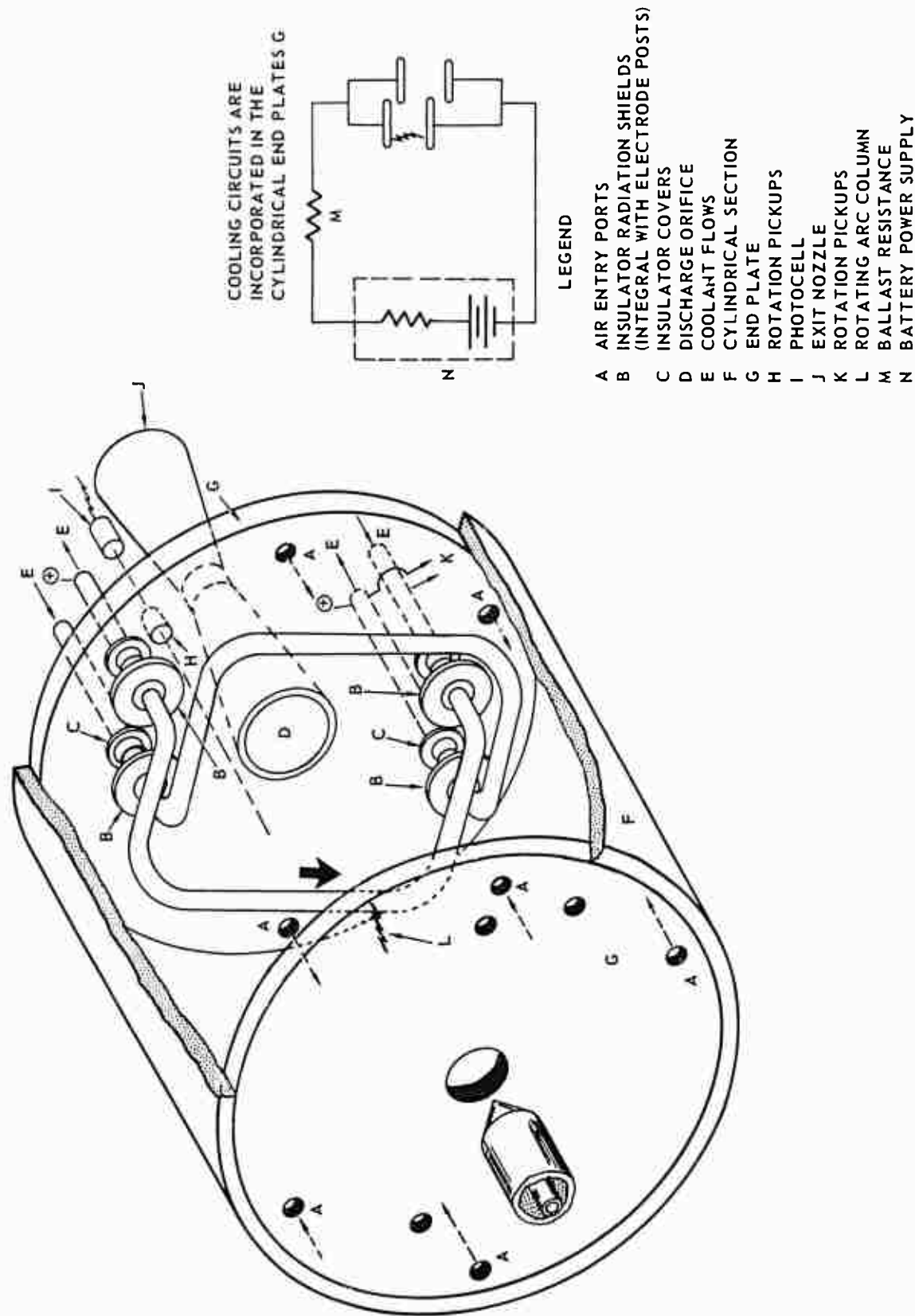


Fig. 1 DIAGRAMMATIC CUTAWAY VIEW OF ARC AIR HEATER

metering, and the second, the discharge orifice (which served when required as the throat of a supersonic nozzle), was also used for enthalpy measurement, provided that the double condition for choking flow

$$(1/0.548)P_{\text{ambient, cold}} < P_{\text{chamber, hot}} < 0.528P_{\text{upstream, cold}}$$

could be satisfied during running.\* Process air entered the unit mainly through eight holes distributed around the periphery of the chamber; a proportion of the air was also allowed to enter through the insulators to promote a plasma-free region around the points where the electrode stems passed out of the chamber. If the whole air flow had been introduced inside the annular arc path, it would then have been free to make a short cut to the discharge orifice without participating effectively in the heating process.

The various cooling channels were provided with inlet and outlet thermocouples and flow meters of the drag disk type. The outputs of these (together with that of an entry-air thermocouple) were scanned every 2.25 sec by a digital data acquisition system and the results recorded on magnetic tape for subsequent reduction in the form of a progressive heat balance.

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\*

The factors 0.528 or 0.548  $\left[ = \left( \frac{\gamma+1}{2} \right)^{-\gamma/(\gamma-1)} \right]$ , appropriate to either "cold" or "hot" air, may be as high as 0.8 if a diffuser is fitted to extend the sonic orifice (Ref. 15).

3.2 Electrode Design--For a short, easily variable electrode gap,\* a facing configuration is convenient in the absence of the need for an external magnetic field. Experience has clearly demonstrated the advantages of such electrodes being constructed of straight lengths of tubing; the actual form used being that of a square with rounded corners. This preserved the required ring character while eliminating the radial magnetic field necessary to counteract the radial component of induced magnetic field that causes the "bowing out" of an arc observed with electrodes having purely radial symmetry. The electrode system, which was cooled by high velocity water (Ref. 14), comprised two pairs of interleaving hollow copper arms, each pair projecting from one of the end plates; the gap between the pairs of arms was normally set at 1-1/4 inch, but larger or smaller values could be used, depending on the discharge voltage required. Each end plate thus supported four electrode posts. These posts were mounted in lucite insulators protected by covers made of fused silica or nonhygroscopic boron nitride; these covers were, in turn, shielded from direct arc radiation by "skirts" formed integrally with the electrode posts. No problem arose as a result of cooling connections forming numerous high-impedance, parallel leakage paths to ground.

3.3 Arc Rotation Measurement--Two different devices were used:

1. In the Original arrangement (Ref. 16), a photocell looked obliquely (i. e., slightly off-axis) through the chamber exit orifice towards a point on or near the annulus swept by the arc, and thus picked up light level changes as the arc rotated. For the present

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\* As a matter of terminology, the word "gap" is used here to describe the distance between positive and negative electrodes, while "split" refers to the much shorter distance between the parallel overlapped arms of the same electrode.

type of chamber, this arrangement was preserved in principle, but the photocell was arranged to look through a window (Ref. 9) in the wall of the arc chamber in a direction tangential to (and at right angles to) both electrodes (Fig. 1). \*

2. The inductive pulse developed as the arc jumped an electrode split was later isolated and suitably filtered to pass only a signal in the frequency range of arc rotation (Fig. 2(a)). In an improved form of the circuit (Fig. 2(b)) a neon lamp/photocell pickup was substituted for the isolation transformer. The electrodes thus acted as their own search coil. Figure 2 (c) shows a typical output trace generated by the latter form of circuit. †

3.4 Stagnation Temperature/Enthalpy Measurement--Three methods of stagnation air temperature measurement were employed:

1. Heat Balance. A computer program was used to determine the summation of losses from the water flows and their respective temperature rises. If the flows in the various channels are  $w_1, w_2, \dots$  and the respective temperature rises are  $\Delta T_1, \Delta T_2, \dots$ , the program determined  $|w\Delta T|$ , where

$$w\Delta T = [w_1, w_2 \dots w_i] \begin{bmatrix} \Delta T_1 \\ \Delta T_2 \\ \cdot \\ \cdot \\ \Delta T_i \end{bmatrix}$$

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\* A similar arrangement has since been used elsewhere (see, e. g., Ref. 17).  
† The author acknowledges the assistance of his colleagues R. T. Cusick and M. E. Rose in the development of these circuits.



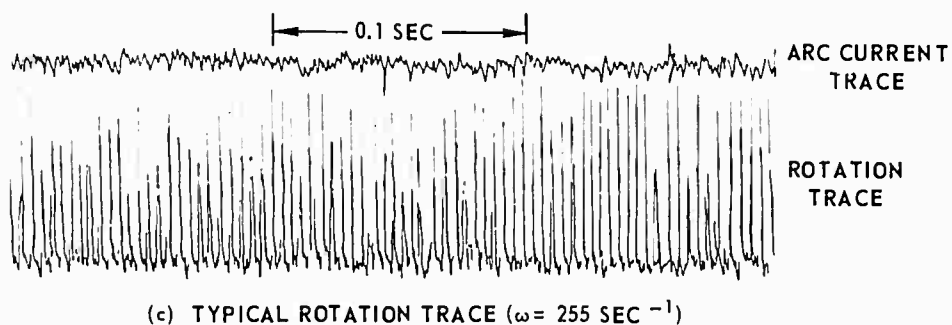
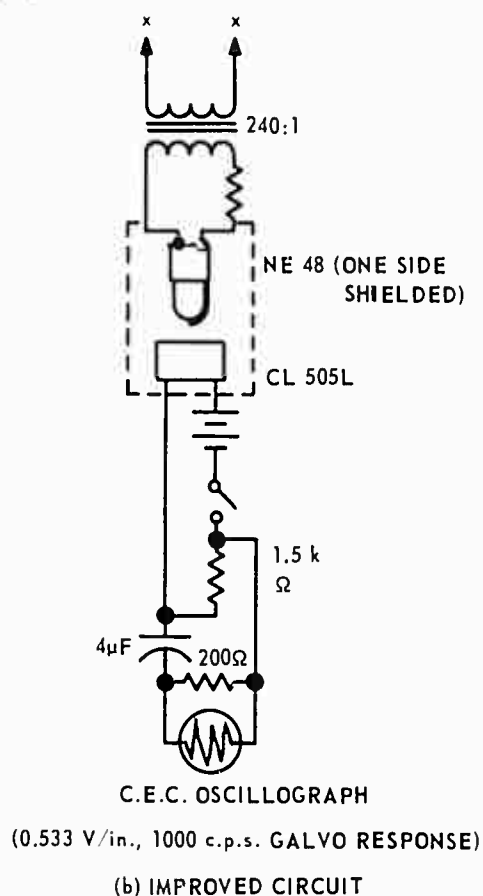
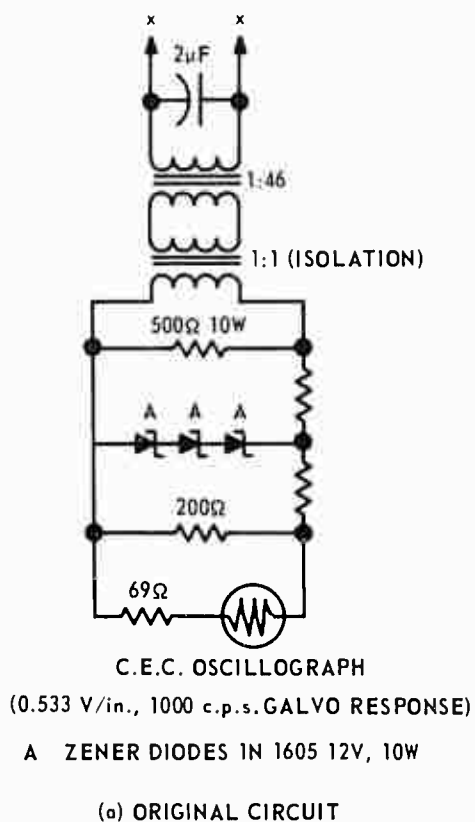
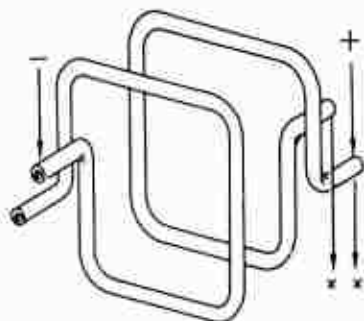


Fig. 2 INDUCTIVE ROTATION MONITORING CIRCUIT

Values of  $w_1 \Delta T_1, \dots, w_i \Delta T_i$  were printed out. This computation was performed every scan, several scans being necessary for thermal equilibrium to be established. The overall efficiency was then given by

$$\eta = 1 - \frac{c_p w \Delta T}{\overline{VI}},$$

where analogue data were used to obtain the mean input power  $\overline{VI}$  from separate voltage and current records. The total (bulk) enthalpy was determined from

$$H_t = H' + \frac{\overline{VI} \eta}{\dot{m}},$$

where  $H'$  is the enthalpy of the incoming air. Appropriate charts were then used to convert from enthalpy to temperature (Ref. 18).

2. Pressure Measurement. (a) For one-dimensional sonic flow from the arc chamber, total enthalpy may be determined from the arc chamber parameters by means of the expression (Refs. 18 and 19)

$$\frac{\dot{m}}{P_t A_{ex}^* C_{d_{ex}}} = \frac{280}{H_t 0.387} \text{ lbm sec}^{-1} \text{ atm}^{-1} \text{ ft}^{-2},$$

which is almost independent of pressure level. Unfortunately,  $C_{d_{ex}}$  is difficult to determine accurately under "hot" conditions; it is associated with a value of  $Re$  based on throat diameter reduced about ten-fold over the cold value, but the actual increase of  $C_{d_{ex}}$  over the cold value is slight (about 2%). (b) Winovich

(Ref. 19) has shown how the enthalpy of the hot condition may be evaluated from the expression

$$\frac{(P)_{t \text{ hot}}}{(P)_{t \text{ cold}}} = \frac{[\dot{m}/A^*_{\text{ex}} P_t C_{d_{\text{ex}}}]_{\text{cold}}}{[\dot{m}/A^*_{\text{ex}} P_t C_{d_{\text{ex}}}]_{\text{hot}}}$$

$$= \frac{\text{constant}}{[\dot{m}/A^*_{\text{ex}} P_t]_{\text{hot}}} \cdot \frac{C_{d_{\text{ex, adiabatic}}}}{C_{d_{\text{ex, diabatic}}}}$$

A heat transfer effect and boundary-layer correction can be taken into account to afford an estimate for the ratio of adiabatic to diabatic  $C_d$ 's. This approach was used to obtain the best comparison with heat balance results for runs using different exit orifices, even though the orifice geometry differed somewhat from that assumed for the boundary-layer calculation. It is obvious that very strong values of swirl can so alter  $C_d$  (Ref. 20) as to vitiate this approach.

3. Pyrometer and Ablating Probe. For certain tests an ablating probe of a material such as graphite was inserted in the jet and observed with a miniature photovoltaic pyrometer (Ref. 21). Such observations gave a lower limit to the stagnation temperature of the jet; the subliming temperature of the material however imposed an upper limit on the measurement that could be obtained.

#### 4. PONDEROMOTIVE FORCE AND AERODYNAMIC DRAG

Radial magnetic field effects associated with the four, 90° electrode corners are here disregarded. The electrodes were considered to be infinitely long straight conductors carrying current. Considering the electrode system shown in Fig. 3, the field at distance  $r$  from one conductor due to current flowing through the electrode up to the arc is, for  $B_z = H_z$  in air,

$$B_z = \frac{1}{2} \frac{2I_y}{10r} \text{ lines cm}^{-2},$$

where  $I_y$  is in amperes and  $r$  is in cm. On an element,  $dr$ , of an arc carrying a current  $I_x$ , the force is

$$\frac{B_z I_x dr}{10} \text{ dynes}.$$

[Note that  $B_z I_x$  is the only significant term in the vector

$$\vec{B} \times \vec{I} = \vec{i}(I_y B_z - I_z B_y) + \vec{j}(I_z B_x - I_x B_z) + \vec{k}(I_x B_y - I_y B_x).]$$

Over the whole length,  $\ell$ , of the arc path the force is

$$\frac{I^2}{100} \int_R^{a-R} \left( \frac{1}{r} + \frac{1}{a-r} \right) dr = \frac{I^2}{100} \left[ \ln \left( \frac{a-R}{R} \right)^2 \right] = \frac{I^2}{100} \left[ \ln \left( \frac{\ell+R}{R} \right)^2 \right] \text{ dynes}.$$

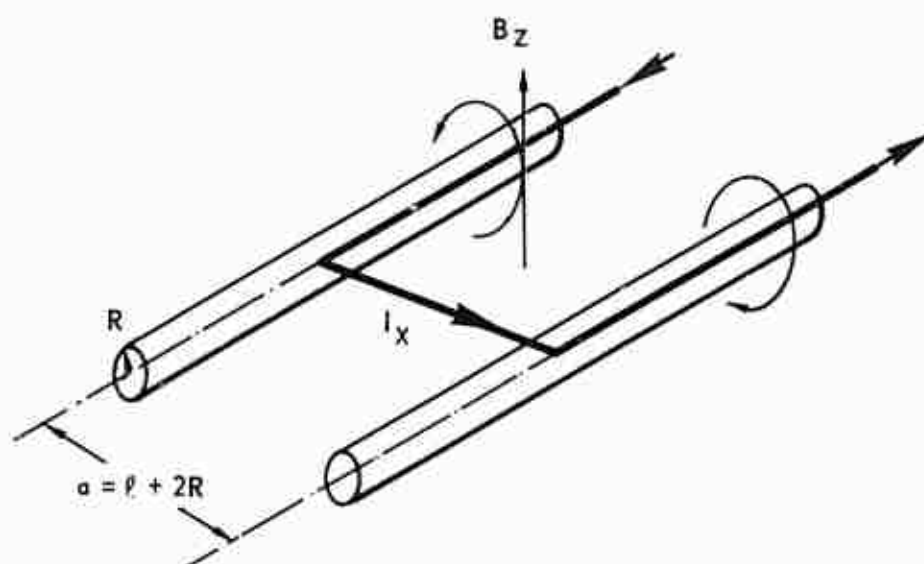


Fig. 3 CURRENT FLOW BETWEEN PARALLEL RECTILINEAR ELECTRODES

Considering an arc as a cylinder of diameter,  $d$ , and length,  $\ell$ , opposed by an aerodynamic drag force,

$$\frac{I^2}{100} [2 \ln \left( \frac{\ell+R}{R} \right)] = \frac{1}{2} C_d \rho \ell d V^2 ;$$

hence, 
$$V = \frac{I \sqrt{2}}{10 \sqrt{C_d \rho \ell d / f(\ell)}} , \quad (1)$$

where  $f(\ell) = 2 \ln [(\ell+R)/R]$ .

Substituting  $\rho = P/RTZ$  in Eq. (1),

$$V = \frac{I}{10} \sqrt{\frac{2 T f(\ell) R Z}{P \ell d C_d}} = \omega \mathcal{L} , \quad (2)$$

where  $\mathcal{L}$  is the arc perimeter track and  $\omega$  the number of arc rotations per second.

The determination of the appropriate value of the length  $\mathcal{L}$  of the arc track was made on the basis of the plan views shown in Fig. 4, which indicate the basic values chosen for the two extreme forms of electrode used. Observation of electrode discoloration and of films of arc behavior indicated that, for example, the curved parts of the posts (out of the main electrode plane) also shared to some extent in conveying current, but it was difficult to make adequate allowance for this. The velocity,  $V$ , is a low subsonic value as far as hot gas is concerned, so that  $T \approx T_t$  and  $P \approx P_t$ . To make the ratio  $f(\ell)/\ell$  equal to unity at the standard value of gap, one may write

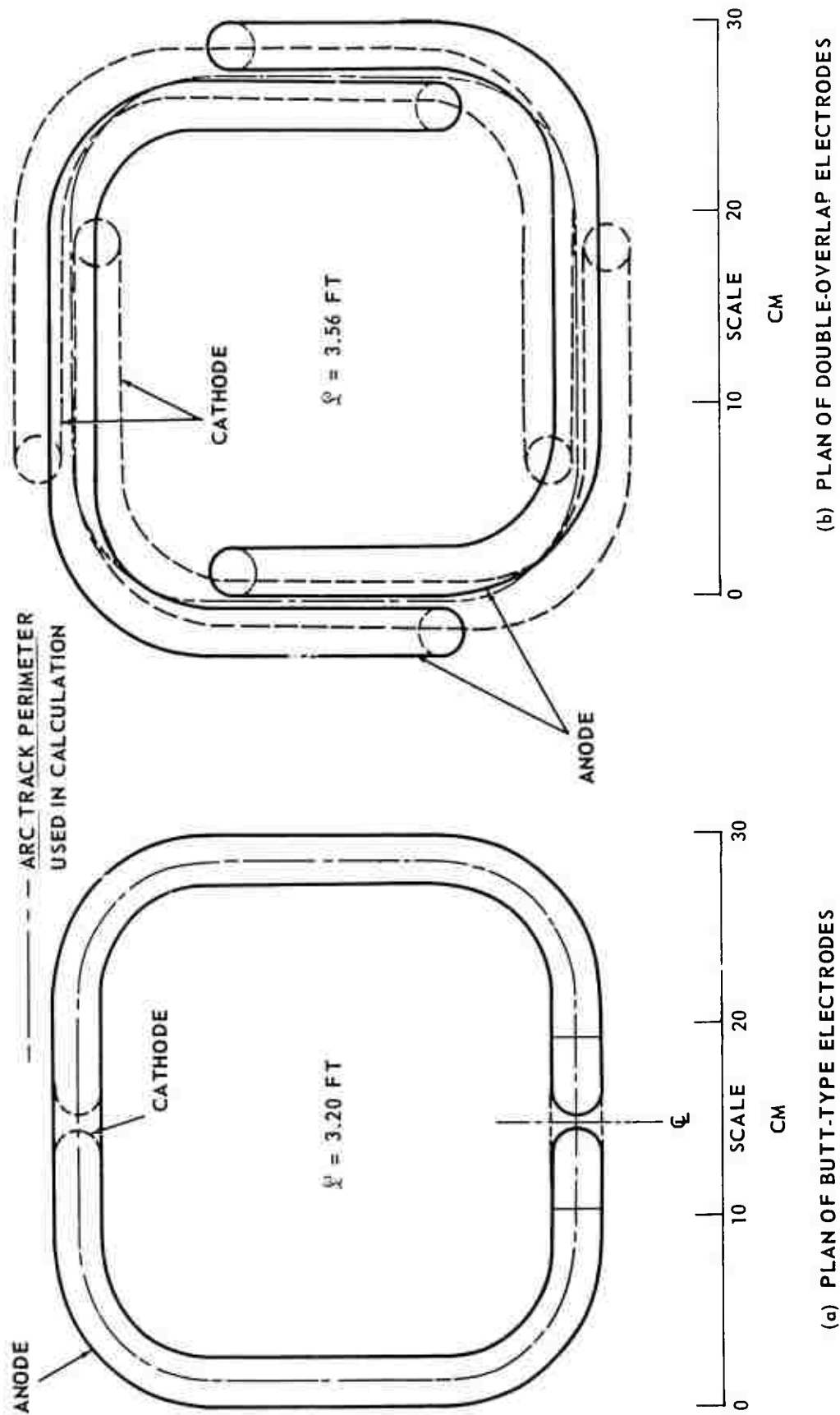


Fig. 4 CALCULATION OF ARC TRACKS

$$\frac{\omega \mathcal{L}}{L \sqrt{T_t}} \sqrt{\frac{f(\ell_o)}{\ell_o f(\ell)}} = C P_t^{-\frac{1}{2}}, \quad (3)$$

$$\text{where } C = \frac{1}{10} \sqrt{\frac{2 R Z f(\ell_o)}{C_d d \ell_o}}.$$

Points representing the value of the first term in Eq. (3) are plotted in Fig. 5. Scatter is ascribed partly to lack of precision in calculating  $\mathcal{L}$  and partly to the fact that average rotation rates have been used. Where the rotation rate was steady, the value is not in question, but occasional "hold-ups" reduced an otherwise steady rate. The line of best fit, drawn at a slope of  $-\frac{1}{2}$ , is used to obtain an experimental value of  $C$ . The bifurcation occurring with overlapped electrodes is also believed to contribute to a small lowering of the rotational velocity, following a current reduction in the separate limbs of an overlap.

For an open air arc, Eq. (2) cannot be further reduced, but, for a choking arc,  $P_t = P_t(\dot{m}, T_t)$ . Further manipulation did not appear to be justified, however, as the parameters controlling rotation were considered to be established.

It is of interest to determine the value of  $d$  from the above expression. Assuming  $C_d = 2$  (flat plate), a typical value of  $d$  was 4.86 cm. From observation of the luminous column (Fig. 6(b)),  $d \approx 5$  cm.

4.1 Rotation Breakdown at Extended Gap--Since the field is much weaker midway between the split-ring electrodes, operating at relatively wide gap, than at the edges of the electrodes, the concept of the arc as a solid body will lead to an imbalance of driving field and opposing force in the central portion of such a gap. The validity of



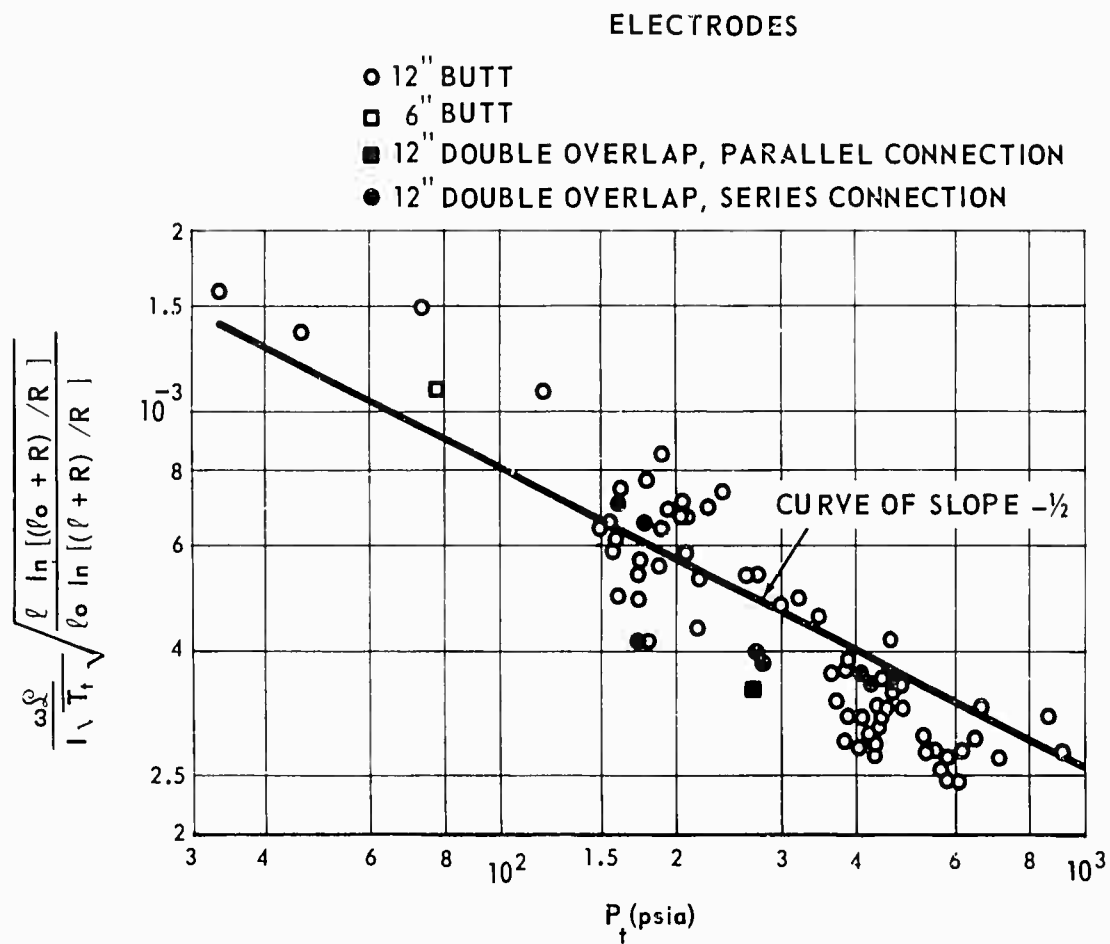


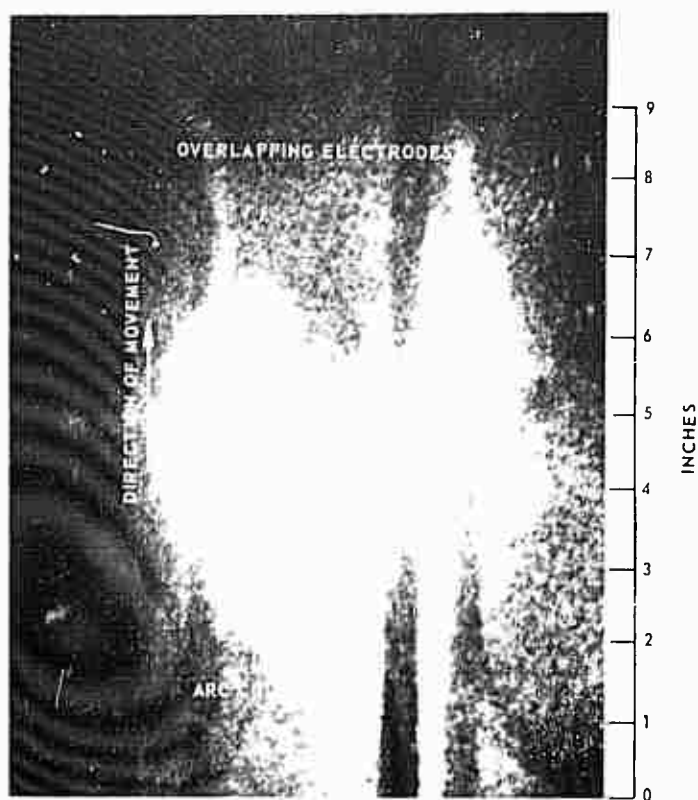
Fig. 5 ROTATION RATE CORRELATION

the expression for arcs of different horizontal lengths was therefore investigated experimentally. The arc shown in Fig. 6(a) ( $\ell = 3$  inches) was being dragged along by its roots (the actual arc image is blurred because of the length of exposure of one frame of the film), but when the gap was extended beyond about 6 inches, the rotational behavior became irregular. Figure 6(b) illustrates a "long" ( $\ell = 18$  inches) gap where the rotation in the central region has collapsed. In such a case, the precise mode of attachment of the arc to the electrodes was not clear; it appeared quasi-diffuse, with vestigial rotation. The impression was given that the form the electrode structure could take was arbitrary since arc filaments were seen to attach at almost any conducting point. (From other evidence, however, it is not believed that the electrode form is arbitrary.) It is probable that such unrotated arcs as those of Eschenbach, et al. (Ref. 22) are of this long type.

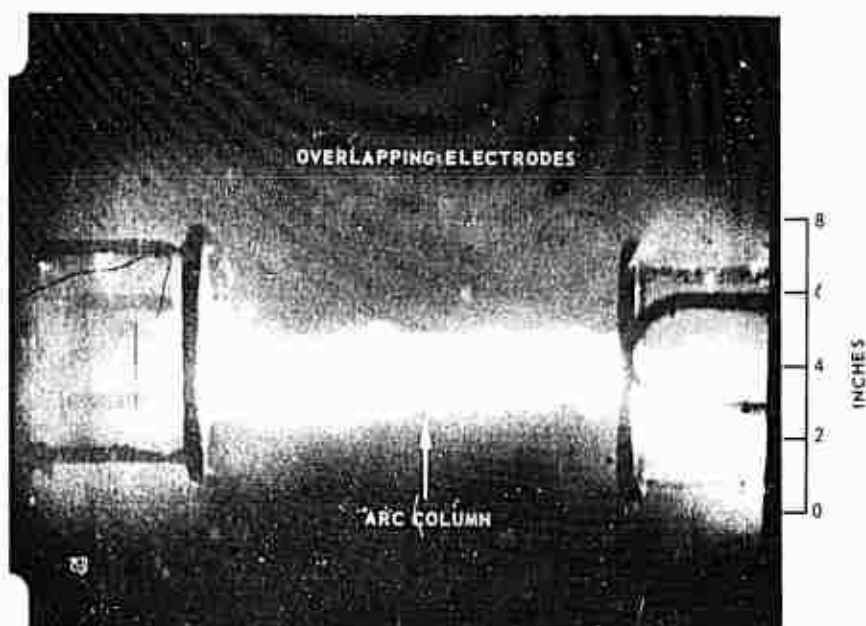
In view of the change of character of the arc as the gap was raised, measurements of voltage versus gap were made at atmospheric pressure, using the apparatus shown in Fig. 6(b). It was deduced that there was no significant voltage change as the arc character changed from short to long, the consistent relationship being

$$v \propto \ell^{0.45}$$

nor was any significant difference in the gap/voltage relationship between butt and overlapped types of electrodes observed.



(a) SHORT GAP  
(PRINTED THROUGH RED FILTER)



(b) LONG GAP  
(PRINTED THROUGH DOUBLE YELLOW FILTER)

Fig. 6 TYPICAL APPEARANCE OF ARC COLUMN

## 5. ANALYSIS OF HEAT LOSSES

In general, three major sources of loss of input energy occurred: (a) radiation from the arc itself; (b) radiation from the volume of gas in the chamber; and (c) forced convective heat transfer from the gas swirl set up by arc rotation. These energy losses were all absorbed by the cooling water. In one set of experiments (Ref. 23) where radiant energy calculations for a high pressure (rotating) arc were quoted, losses other than radiation were neglected so that the energy balance was given by

$$\dot{m} \Delta H = P - IV ,$$

where  $\Delta H$  = enthalpy addition,

$I$  = intensity of radiation per unit volume (radiated into  $4\pi$  steradians),

$V$  = chamber volume, and

$P$  = heat power input.

However, although the claim was made that the experimental results fell amazingly close to theory, it was clear from an examination of the plotted points that the temperatures were so low that the corresponding "radiation-loss" lines had not, or had hardly, diverged from the "no-radiation-loss" line. Since then  $IV \approx 0$ , nothing was proved regarding coincidence of experimental results and theory, which was unfortunate since any experimental evidence of a contamination effect was of considerable interest. It was felt that this particular basic assumption

offered no guidance, and it was therefore necessary to approach the problem by a different route.

5.1 Arc Radiation -- The individual heat loss by radiation from an arc is difficult to estimate. From observation of the thermal attack on the cylindrical section of an earlier steel arc case, and from the general ablation pattern on boron nitride liners on smaller arc units, the main effect was seen across a band about 2 inches wide on the cylindrical section immediately outside the path of the arc. The proportion of heat lost in this way was believed to be small in proportion to the rest, except possibly in the case of the electrodes. An assessment of the importance of the direct radiation in the total heating was made indirectly by the following experiment.

In an attempt to improve efficiency by absorbing as much as possible of the radiation emitted by the arc itself, the effect of injection of a relatively small quantity of absorbent (< 10% of air flow by weight) was investigated. A powder feeder originally designed for handling alumina was adapted for use with graphite (which acts as its own lubricant). The results of runs of long duration are shown in Fig. 7; the running conditions are given in Table I. The figure shows that the heat loading on the case was increased while the gas enthalpy was decreased by graphite injection,

Table I  
Arc Conditions for Graphite Injection Runs

Run	Air Flow Rate, pps	Powder Flow Rate, pps	$P_t$ , psia	Input Power, MW	
				Powder Off	Powder On
271	0.41	0.025	23	2.04	1.92
272	0.41	0.017	23	2.04	1.87
273	0.41	0.012	23	2.04	1.89
274	0.41	0.033	23	2.03	1.87

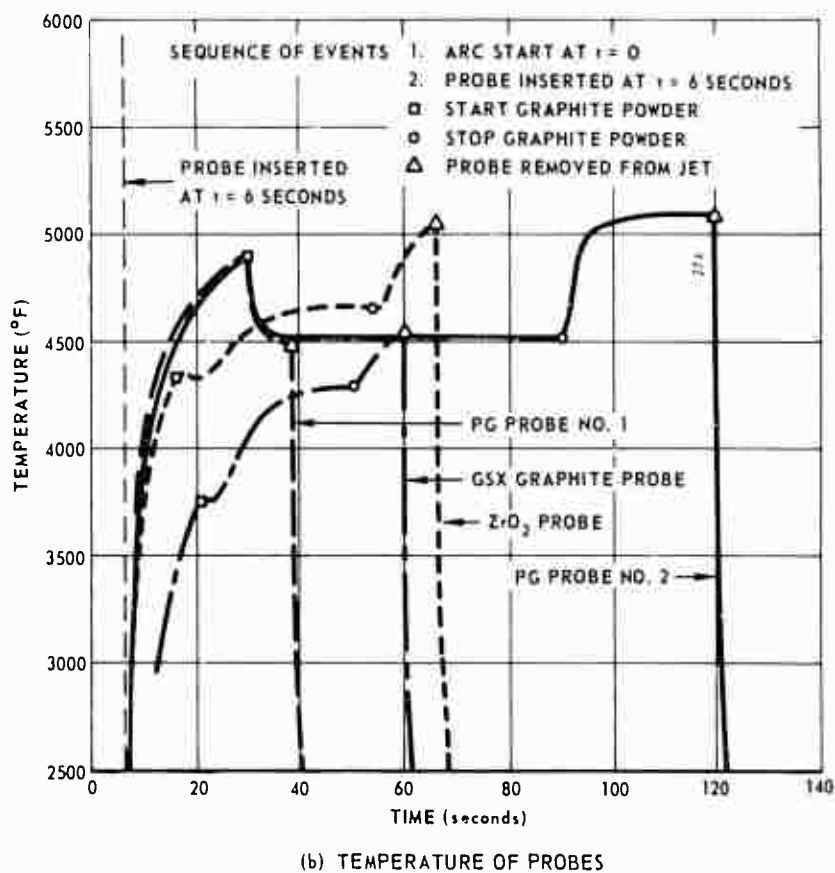
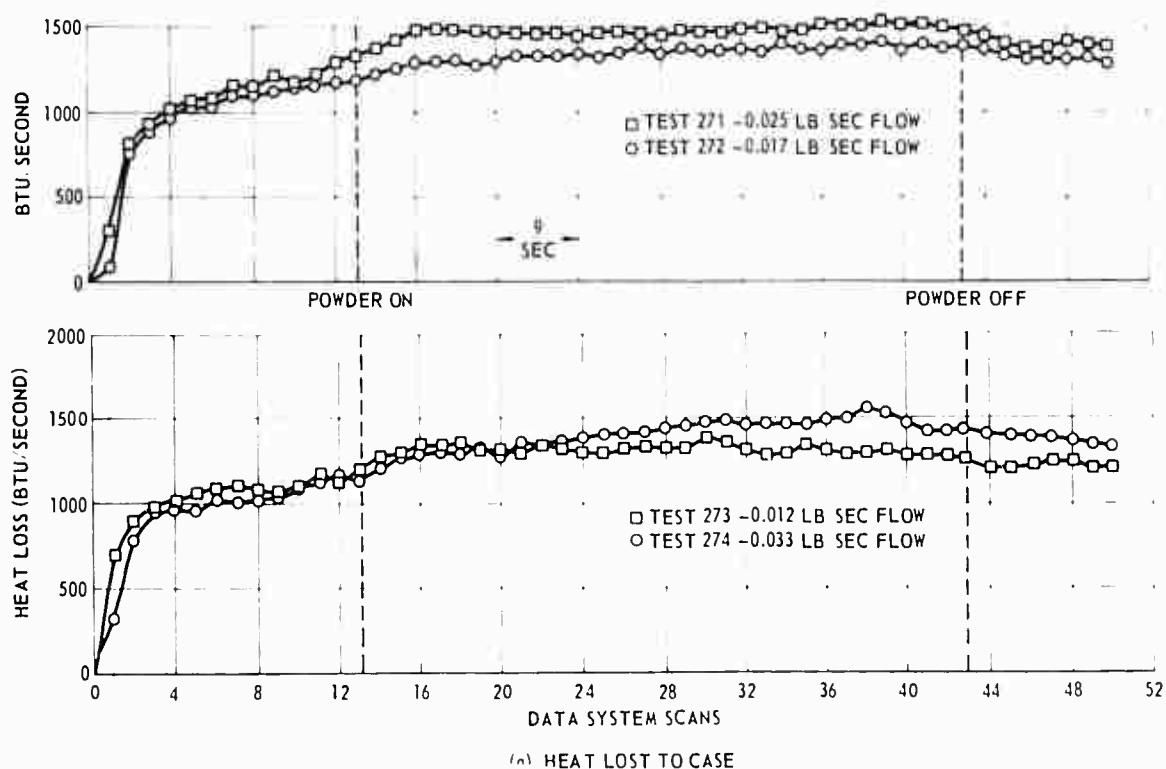


Fig. 7 CONDITIONS DURING GRAPHITE INJECTION

the latter effect being checked by means of the pyrometer-and-ablating-probe method of temperature measurement, using graphite and zirconia samples.\* This result indicated that the general gas radiation was increased by graphite injection (probably due to the carbon monoxide bands). Observation of the emerging jet showed an increase in luminosity in the red region. From the high opacity of the (cold) carrier gas, and the fact that a large amount of graphite passed through the arc without being burned up, it was concluded that, though the graphite was probably an effective absorber of arc radiation, the effect of the arc radiation was small compared to that of the radiation emanating from the gas itself. This conclusion was strengthened by the fact that the overall efficiency of an arc unit could be caused to vary between about 5 and 50% by suitable choice of running conditions (see below) even though the power input varied little. To test this hypothesis arc radiation was therefore neglected in the analysis to follow.

5.2 Forced Convection -- It had previously been suggested that the swirl imparted to the gas by an arc affected the heat transfer (Ref. 7). This was specifically demonstrated by short-circuiting part of the ballast resistance during certain runs<sup>†</sup> so that the current (and therefore the rotation rate) was caused to increase by a relatively large amount (about 25%). The chamber pressure remained almost constant throughout the runs, showing that a decrease in efficiency almost

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\* Acknowledgment is made to Messrs. M. L. Hill and J. M. Akridge for their assistance in this part of the program and to Dr. W. H. Avery for his original suggestion regarding this approach.

<sup>†</sup> The runs designated 5 and 6 in Table II represent the earlier and later conditions of such a run.

compensated for the increase in input power ( $\propto$  current, since the voltage did not change under these circumstances). Corresponding effects were produced in a unit in which an external field could be varied to change the rotation rate at constant current. When the overall efficiency was plotted against the rotation rate, a strong connection emerged, which transcended the individual effects of pressure and current (Fig. 8).

Consider now the simple vortex flow model shown in Fig. 9. Let  $r_2$  be the radius of the circle whose circumference is equal to the arc track, computed as indicated above, and let  $r_3$  and  $r_1$  be the radius of the cylindrical chamber wall and that of the exit duct, respectively. The induced vortex  $rV = \text{constant}$  ( $r_2 < r < r_3$ ) gives

$$V = 2\pi r_2^2 \omega / r ,$$

and therefore,

$$V_3 = \pi \frac{d_2^2}{d_3} \omega .$$

The air velocity  $V_2$  is here assumed to be equal to  $\omega \mathcal{L}$ , where  $\omega$  is now considered to be a uniform angular velocity. For example, for  $\omega = 100 \text{ sec}^{-1}$  and  $d_2 = 1.13 \text{ ft}$ ,  $V_3 = 207 \text{ ft sec}^{-1}$ . For the forced vortex ( $r_1 < r < r_2$ ),

$$V = 2\pi r \omega .$$

The variation of velocity in the respective vortices is sketched in relation to the superimposed axes in Fig. 10.



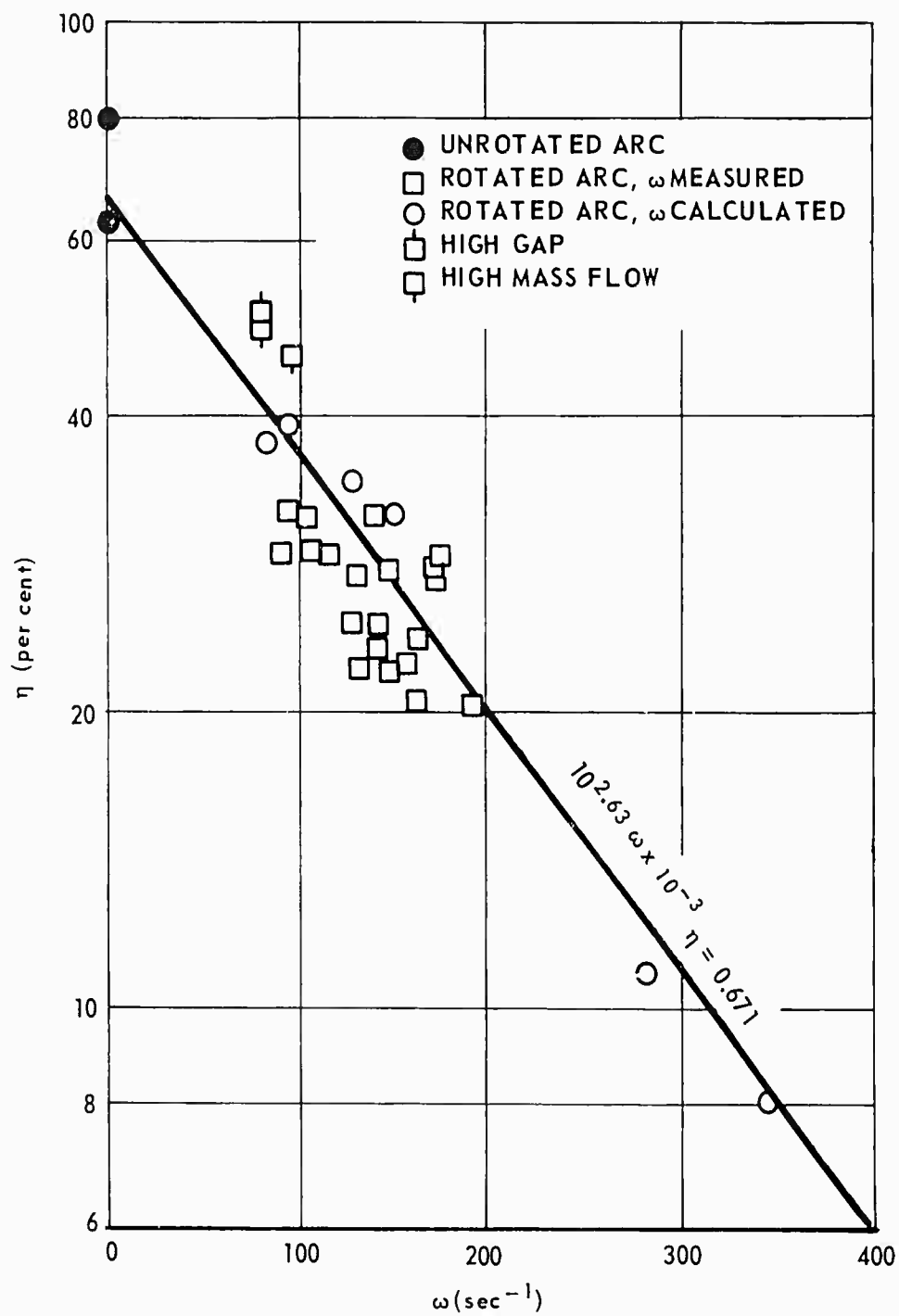


Fig. 8 ROTATION RATE VS OVERALL EFFICIENCY

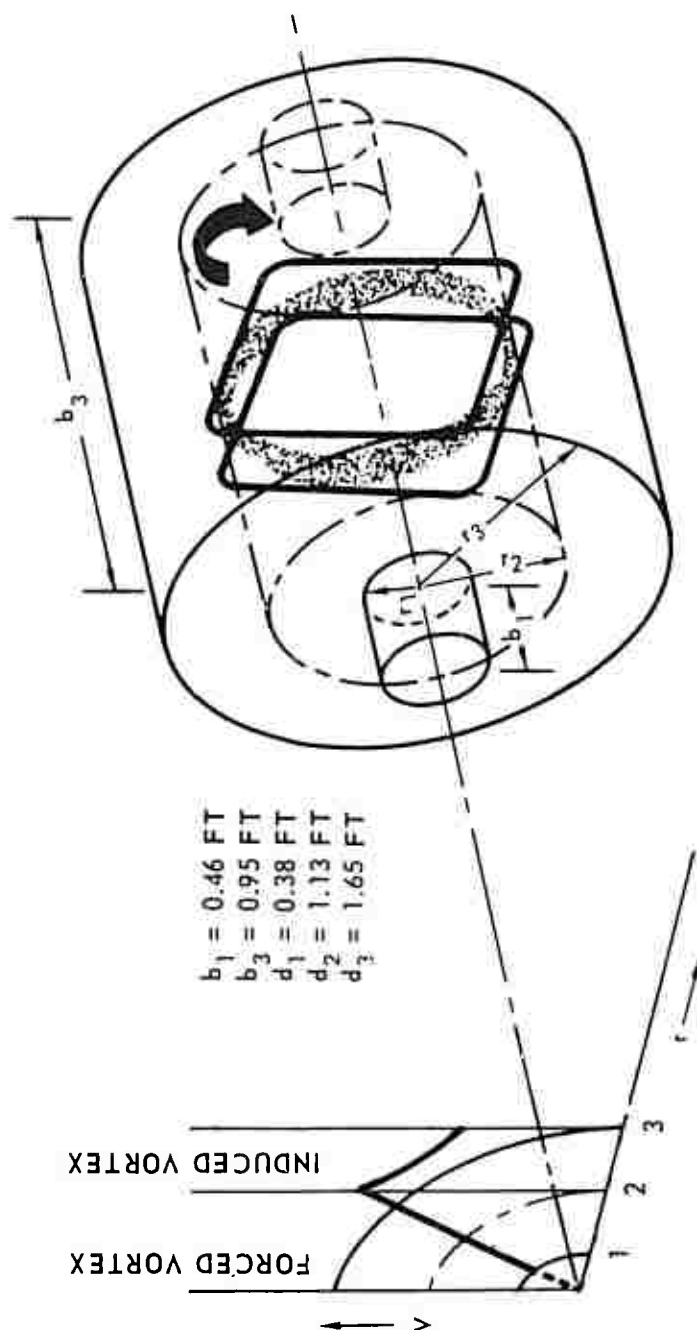


Fig. 9 MODEL OF VORTEX FLOW IN ARC CHAMBER

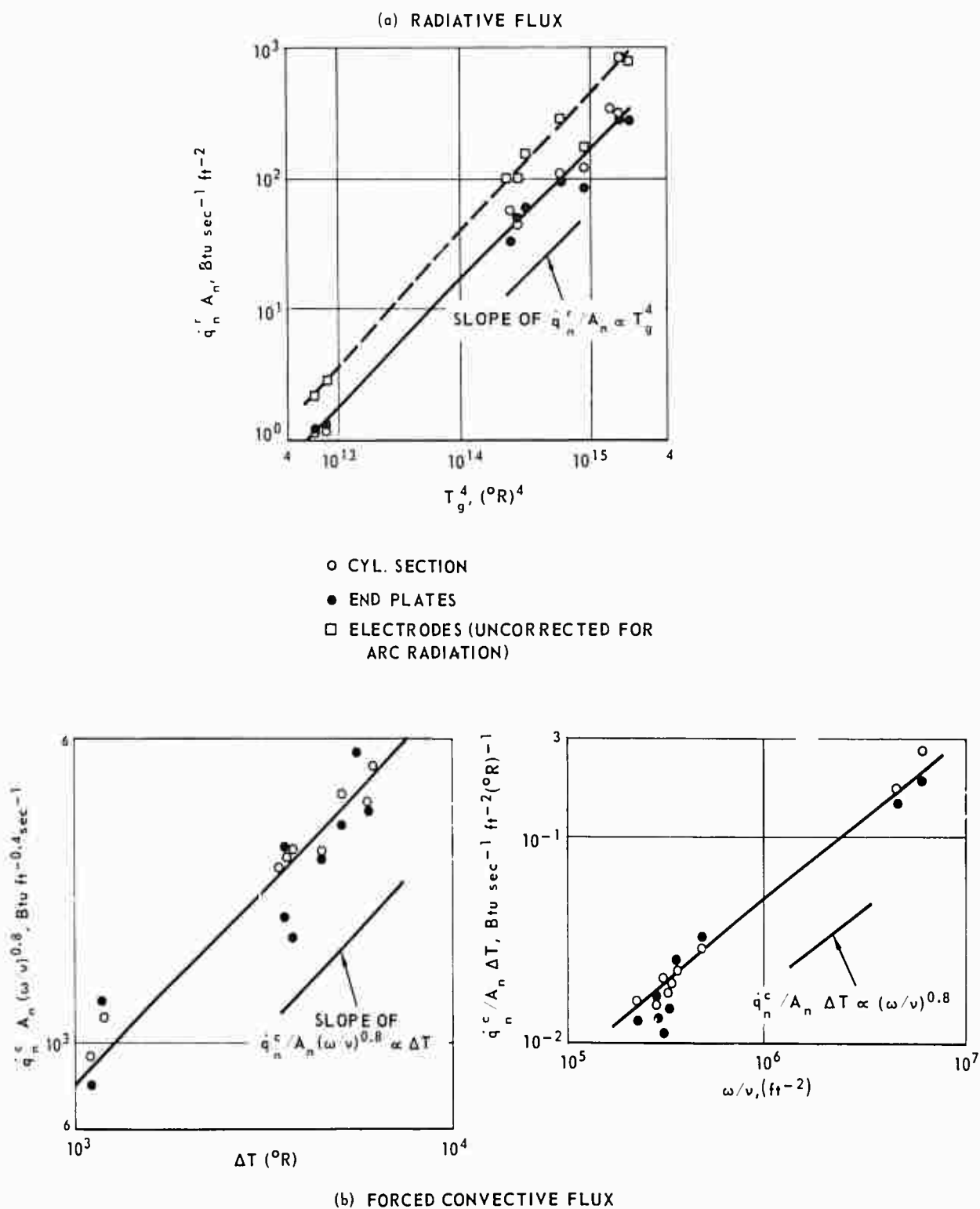


Fig. 10 CERTAIN SOLUTIONS FOR PROPORTION OF RADIATIVE AND CONVECTIVE FLUX

The heat flux to the walls may be simply expressed in terms of enthalpy and Stanton number as

$$A\dot{q} = St \dot{m} \Delta H ,$$

but in the case under consideration, the value of  $\dot{m}$  is not defined. Instead, therefore, recourse was had to the Dittus and Boelter form of correlation:

$$Nu = C (Re)^{0.8} (Pr)^{0.33} , \quad (4)$$

where the constant normally has the value 0.023. The characteristic length in the Reynolds and Nusselt numbers was defined by  $4r_h$ , where  $r_h$  is the hydraulic radius, as follows:

1. Cylindrical Section or Exit I et.

$$r_h = \frac{\text{volume of chamber}}{\text{heat transfer area}} = \frac{\pi d_3^2 b_3}{4\pi d_3 b_3} = \frac{d_3}{4} \text{ or } \frac{\pi d_1^2 b_1}{4\pi d_1 b_1} = \frac{d_1}{4} .$$

$$\therefore 4r_h = d_3 = 19.75 \text{ inches or } d_1 = 4.50 \text{ inches.}$$

The volume occupied by the electrodes was neglected as being small compared with that of the chamber (< 2% error).

2. End Plate.

$$r_h = \frac{\text{volume of annulus}}{\text{heat transfer area}} = \frac{2\pi r b_3 \Delta r}{2(2\pi r \Delta r)} = \frac{b_3}{2}.$$

$$\therefore 4r_h = 2b_3 = 22.88 \text{ inches.}$$

3. Electrode.

$$r_h = \frac{\text{cross-sectional area}}{\text{wetted perimeter}} = \frac{\pi R^2}{2\pi R} = \frac{R}{2}.$$

$$\therefore 4r_h = 2R = 1 \text{ inch.}$$

The appropriate velocity may now be introduced into the Reynolds numbers for the various cases:

1. Cylindrical Section (induced vortex).

$$h = \frac{kC}{d_3} (Pr)^{0.33} \left( \frac{d_3 V_3}{\nu} \right)^{0.8}.$$

Dropping the stagnation subscript, since  $T \approx T_t$ ,

$$\dot{q}_{\text{cyl, induced}}^c = Ah\Delta T = f(\dot{q})_{\text{cyl, induced}} (\omega/\nu)^{0.8} \Delta T = f(\dot{q})_{\text{cyl, induced}} f^c(T),$$

(5)

$$\text{where } f(\dot{q})_{\text{cyl, induced}} = \pi b_3 kC (Pr)^{0.33} (\pi d_2^2)^{0.8}.$$

2. End Plate (induced vortex).

$$h = \frac{kC}{2b_3} (Pr)^{0.33} \left( \frac{2b_3 V}{\nu} \right)^{0.8}.$$

$$\begin{aligned} \therefore \dot{q}_{\text{end, induced}}^c &= \int_2^3 2\pi r h \Delta T dr \\ &= f(\dot{q})_{\text{end, induced}} (\omega/\nu)^{0.8} \Delta T = f(\dot{q})_{\text{end, induced}} f^c(T), \end{aligned} \quad (6)$$

$$\text{where } f(\dot{q})_{\text{end, induced}} = \frac{\pi k C}{1.2 b_3^{0.2}} (Pr)^{0.33} (4\pi r_2^2)^{0.8} (r_3^{1.2} - r_2^{1.2}).$$

3. End Plate (forced vortex).

$$h = \frac{kC}{2b_3} (Pr)^{0.33} \left( \frac{2b_3 V}{\nu} \right)^{0.8}.$$

$$\begin{aligned} \therefore \dot{q}_{\text{end, forced}}^c &= \int_1^2 2\pi r h \Delta T dr \\ &= f(\dot{q})_{\text{end, forced}} (\omega/\nu)^{0.8} \Delta T = f(\dot{q})_{\text{end, forced}} f^c(T), \end{aligned}$$

$$\text{where } f(\dot{q})_{\text{end, forced}} = \frac{\pi k C}{2.8 b_3^{0.2}} (Pr)^{0.33} (4\pi)^{0.8} (r_2^{2.8} - r_1^{2.8}). \quad (7)$$

4. Exit Duct (forced vortex).

$$h = \frac{kC}{d_1} (Pr)^{0.33} \left( \frac{d_1 V_1}{\nu} \right)^{0.8}$$

$$\therefore \dot{q}_{cyl, forced}^c = f(\dot{q})_{cyl, forced} (\omega/\nu)^{0.8} \Delta T = f(\dot{q})_{cyl, forced}^c(T), \quad (8)$$

$$\text{where } f(\dot{q})_{cyl, forced} = \pi b_1 kC (Pr)^{0.33} (\pi d_1^2)^{0.8}$$

5. Electrode (forced vortex).

$$h = \frac{kC}{2R} (Pr)^{0.33} \left( \frac{2R V_2}{\nu} \right)^{0.8}$$

$$\therefore \dot{q}_{elec, forced}^c = A_{elec} h \Delta T = f(\dot{q})_{elec, forced} (\omega/\nu)^{0.8} \Delta T$$

$$= f(\dot{q})_{elec, forced}^c(T), \quad (9)$$

$$\text{where } f(\dot{q})_{elec, forced} = \pi kC p (Pr)^{0.33} (2\pi R d_2)^{0.8}$$

The geometrical factors  $f(\dot{q})_n$  for the various surfaces are constant for a given configuration, the main values being given in Table II.

5.3 Radiation from Chamber Gas--Calculated values of the radiation from normal, optically thin, air, given as the emissivity of a slab per unit thickness ( $\epsilon/L$ ), are available (Ref. 24).<sup>\*</sup> For radiation from shapes other than plane, the total radiation per unit volume is defined as twice these values, since the "plane" then has two sides, namely  $2\sigma(\epsilon/L) T^4$ , where  $\sigma$  is Boltzmann's constant. Calculated values were suspected of being inapplicable; however, when values of  $\dot{q}(\omega/\nu)^{0.8}$  were plotted, they were found to be roughly proportional to  $T^2$ , which suggested that gas radiation represented a larger fraction of the total radiation than would have been the case for pure air at the temperature of operation. It is known that contaminants could change gas emissivity by a factor of from 2 to 10 (Refs. 25 and 26).<sup>†</sup>

5.4 Separation of Radiative from Convective Losses--Neglecting direct arc radiation, then separating out quantities depending upon  $T$  and  $\omega$  from the geometrical factors, we may write for the  $n$ th chamber surface of area  $A_n$ ,

$$\dot{q}_n = x_n^r f^r(T) + x_n^c f^c(T)_n, \quad (10)$$

where the unknown geometrical factors  $x_n^r$  and  $x_n^c$  are given by

$$x_n^r = 2\sigma V(\epsilon/L) A_n / A_{\text{total}},$$

and

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\* A higher actual emissivity than that given by Kivel and Bailey (Ref. 24) seems to be suggested by Ref. 26 (for higher temperature values).

† It is noted that the General Electric Company (Philadelphia) double-Gerdien type of arc employs very pure air, (Ref. 27) in order to minimize radiation losses and so permit operation at the highest possible enthalpy.



$$x_n^c = f(\dot{q})_n.$$

In addition,  $f^r(T) = (T_g^4 - T_w^4)$ , but since black body radiation from the wall can safely be neglected,

$$T_w^4 \ll T_g^4, \text{ so}$$

$$f^r(T) = T_g^4. \quad (11)$$

Also,

$$f^c(T)_n = (T_g - T_w)_n (\omega/\nu)^{0.8}. \quad (12)$$

Equation 10 may thus be written for all runs 1-m and surfaces 1-n for which a heat flux measurement is available:

$$\begin{aligned} \dot{q}_{1n} &= x_n^r f^r(T_1) + x_n^c f^c(T_1)_n \\ &\cdot \quad \cdot \quad \cdot \\ &\cdot \quad \cdot \quad \cdot \\ &\cdot \quad \cdot \quad \cdot \\ \dot{q}_{mn} &= x_n^r f^r(T_m) + x_n^c f^c(T_m)_n \end{aligned}$$

5.5 Results and Discussion--Apart from about 200 earlier runs conducted with steel arc components (not considered here on account of possible inconsistency arising from differing contamination products as the walls underwent ablation during running), 68 runs were made with only a copper cylindrical section, and of these, 24 runs were made with a complete copper shell; subsequently coated components

were used. From these 24 runs a few involving the best possible spread of temperature were selected for analysis. The electrode gap was, of course, sufficiently short in these runs ( $< 2.5$  inches) to ensure that regular rotation occurred. In a calculation designed to illustrate the procedure developed above,  $x^c$  and  $x^r$  were derived by solving pairs of simultaneous equations with far-apart values of  $T$ . A graphical representation of the solution is given in Fig. 10 for the major surfaces, but as expected, the common correlation was not valid for the electrodes. In plotting radiation per unit area for the end plates, the exit sections were not included as these were considered to be in virtual shadow. Where appropriate, values of  $(\epsilon/L)$  and  $C$  were derived from the equations given above, and these are given with other data in Table II. The values of  $(\epsilon/L)$  for the shell were not found to vary much from the mean value of  $0.78 \text{ ft}^{-1}$  over the full temperature range, a value which in nearly all cases was much higher than for pure air, as indicated by the comparison shown in Table II with the fluxes calculated from the information given by Kivel and Bailey (Ref. 24). (The accuracy of this latter calculation is not, however, considered to be high owing to the extrapolation necessary for dense plasmas ( $\rho/\rho' > 1$ ) and to the fact that the graphical presentations in Ref. 24 are not entirely self-consistent.) It is clear from Fig. 10(a) that the radiation flux per unit area on the electrodes far exceeds the average for the shell. It is also proportional to a power of  $T_g$  greater than four. Since the contribution of ohmic heating is negligible in the case of copper electrodes, this discrepancy is ascribed to arc radiation, the presence of which invalidates the solution for the convective flux. Derived values of the convective flux have therefore not been plotted in Fig. 10(b). While Fig. 10(a) suggests that a correction can be made for the arc radiation, this was not performed in the absence of a suitable theory.

Table II  
Major Solutions

Surface	Run No.	$T_t$ °R	$\dot{q}$ Btu sec <sup>-1</sup>	$\dot{q}^R = x^R f^R(T)$ Btu sec <sup>-1</sup>	Calculated Radiation Loss (Ref. 24) Btu sec <sup>-1</sup>	$\epsilon/L$ ft <sup>-1</sup>	$\dot{q}^R/A_n$ Btu ft <sup>-2</sup> sec <sup>-1</sup>	$\dot{q}^C = x^C f^C(T)$ Btu sec <sup>-1</sup>	$\dot{q}^C/A_n \Delta T$ Btu sec <sup>-1</sup> ft <sup>-2</sup> (°R) <sup>-1</sup>	$\dot{q}^C/A_n (\omega/\nu)^{0.8}$ Btu ft <sup>-0.4</sup> sec <sup>-1</sup>	$C = Nu(Re)^{-0.8} (Pr)^{-0.33}$
Cylindrical Section	1	4940	901	514	25	0.857	104	385	$1.76 \times 10^{-2}$	$0.304 \times 10^{-2}$	$2.40 \times 10^{-5}$
	2	6440	1934	1482	469	-	300	552	$1.54 \times 10^{-2}$	$0.407 \times 10^{-2}$	-
	3	3960	671	188	544	0.694	38	483	$2.83 \times 10^{-2}$	$0.282 \times 10^{-2}$	$2.32 \times 10^{-5}$
	4	6680	2201	1514	1570	-	307	687	$2.25 \times 10^{-2}$	$0.505 \times 10^{-2}$	-
	5	1600	952	5.3	0.07	0.765	1.1	947	$1.72 \times 10^{-2}$	$0.914 \times 10^{-2}$	$2.92 \times 10^{-5}$
	6	1680	1532	5.9	0.11	0.706	1.2	1526	$2.61 \times 10^{-2}$	$0.117 \times 10^{-2}$	$3.46 \times 10^{-5}$
	7	4240	638	261	17	0.764	53	377	$2.04 \times 10^{-2}$	$0.315 \times 10^{-2}$	$2.94 \times 10^{-5}$
	8	5500	958	575	97	0.594	117	383	$1.54 \times 10^{-2}$	$0.424 \times 10^{-2}$	$2.91 \times 10^{-5}$
	9	4080	568	225	10	0.764	46	343	$1.94 \times 10^{-2}$	$0.300 \times 10^{-2}$	$2.93 \times 10^{-5}$
End Plates (2)	1	4940	538	303	16	0.892	98	235	$1.71 \times 10^{-2}$	$0.292 \times 10^{-2}$	$0.612 \times 10^{-5}$
	2	6440	1150	875	295	-	282	274	$1.49 \times 10^{-2}$	$0.395 \times 10^{-2}$	-
	3	3960	443	106	342	0.746	34	337	$3.14 \times 10^{-2}$	$0.313 \times 10^{-2}$	$0.647 \times 10^{-5}$
	4	6680	1333	858	989	-	277	477	$2.49 \times 10^{-2}$	$0.551 \times 10^{-2}$	-
	5	1600	510	3.7	0.04	0.868	1.1	506	$14.8 \times 10^{-2}$	$0.0782 \times 10^{-2}$	$0.598 \times 10^{-5}$
	6	1680	699	4.0	0.07	0.865	1.3	695	$18.9 \times 10^{-2}$	$0.0957 \times 10^{-2}$	$0.478 \times 10^{-5}$
	7	4240	320	178	11	0.955	58	142	$1.22 \times 10^{-2}$	$0.189 \times 10^{-2}$	$0.421 \times 10^{-5}$
	8	5500	475	269	61	0.510	8.7	206	$1.33 \times 10^{-2}$	$0.358 \times 10^{-2}$	$0.604 \times 10^{-5}$
	9	4080	297	148	6	0.922	48	149	$1.34 \times 10^{-2}$	$0.207 \times 10^{-2}$	$0.489 \times 10^{-5}$
Electrodes (2)	1	4940	1330	763	-	-	285	567	$4.79 \times 10^{-2}$	$0.824 \times 10^{-2}$	$0.920 \times 10^{-5}$
	2	6440	2887	2203	-	-	822	685	$4.35 \times 10^{-2}$	$1.14 \times 10^{-2}$	-
	3	3960	1204	265	-	-	99	939	$10.20 \times 10^{-2}$	$1.01 \times 10^{-2}$	$1.23 \times 10^{-5}$
	4	6680	3481	2135	-	-	797	1346	$8.12 \times 10^{-2}$	$1.82 \times 10^{-2}$	-
	5	1600	2385	60	-	-	22	2376	$77.2 \times 10^{-2}$	$4.25 \times 10^{-2}$	$1.79 \times 10^{-5}$
	6	1680	2977	7.5	-	-	2.8	2970	$95.6 \times 10^{-2}$	$4.17 \times 10^{-2}$	$1.75 \times 10^{-5}$
	7	4240	940	394	-	-	147	546	$3.94 \times 10^{-2}$	$0.605 \times 10^{-2}$	$1.09 \times 10^{-5}$
	8	5500	1372	450	-	-	168	922	$6.88 \times 10^{-2}$	$1.85 \times 10^{-2}$	$1.79 \times 10^{-5}$
	9	4080	1095	268	-	-	100	827	$8.16 \times 10^{-2}$	$1.33 \times 10^{-2}$	$1.70 \times 10^{-5}$

Table II (Cont'd)  
 Geometrical Factors

$$x^C = f^C(\dot{q}),$$

Surface	Btu ft <sup>1.6</sup> sec <sup>-1</sup> (°R) <sup>-1</sup>	A <sub>n</sub> , ft <sup>2</sup>
Cylindrical section	0.141C	4.93
End plate	0.183C	1.55
Exit duct	0.037C	0.54
Electrode	0.277C	1.34

Chamber Volume = 2.03 ft<sup>3</sup>.

The best correlation of end plate and cylindrical section data for the convective flux per unit area was achieved by omitting the areas of the exit ducts (although these were physically part of the end plates). Values of  $C$  were also plotted in Fig. 11 against  $Re$ , the values of  $Pr$  and  $k$  used being  $0.775$  and  $0.516 \text{ Btu ft}^{-1} \text{ sec}^{-1} (\text{°R})^{-1}$ , respectively. The values obtained for  $C$  are unusually low for such a correlation, but these depend partly on the value chosen for  $k$  (which may be too high, particularly as the surfaces concerned--and especially the electrodes--are operated at high temperatures). In addition, the values of  $Re$  may be artificially high because of the assumption that the gas vortex rotates at the same angular velocity as the arc. A refinement of values is therefore possible. Scatter in all the results reflects inaccuracies in the determination of  $T$ ,  $\omega$ , and  $\dot{q}$ , but the flow model based upon the Dittus and Boelter equation is seen to provide a basic solution for the values of the convective flux, since the major variable in  $\omega/\nu$  is undoubtedly  $\omega$ . Therefore, except for the losses due to arc radiation, a synthesis of losses is possible.

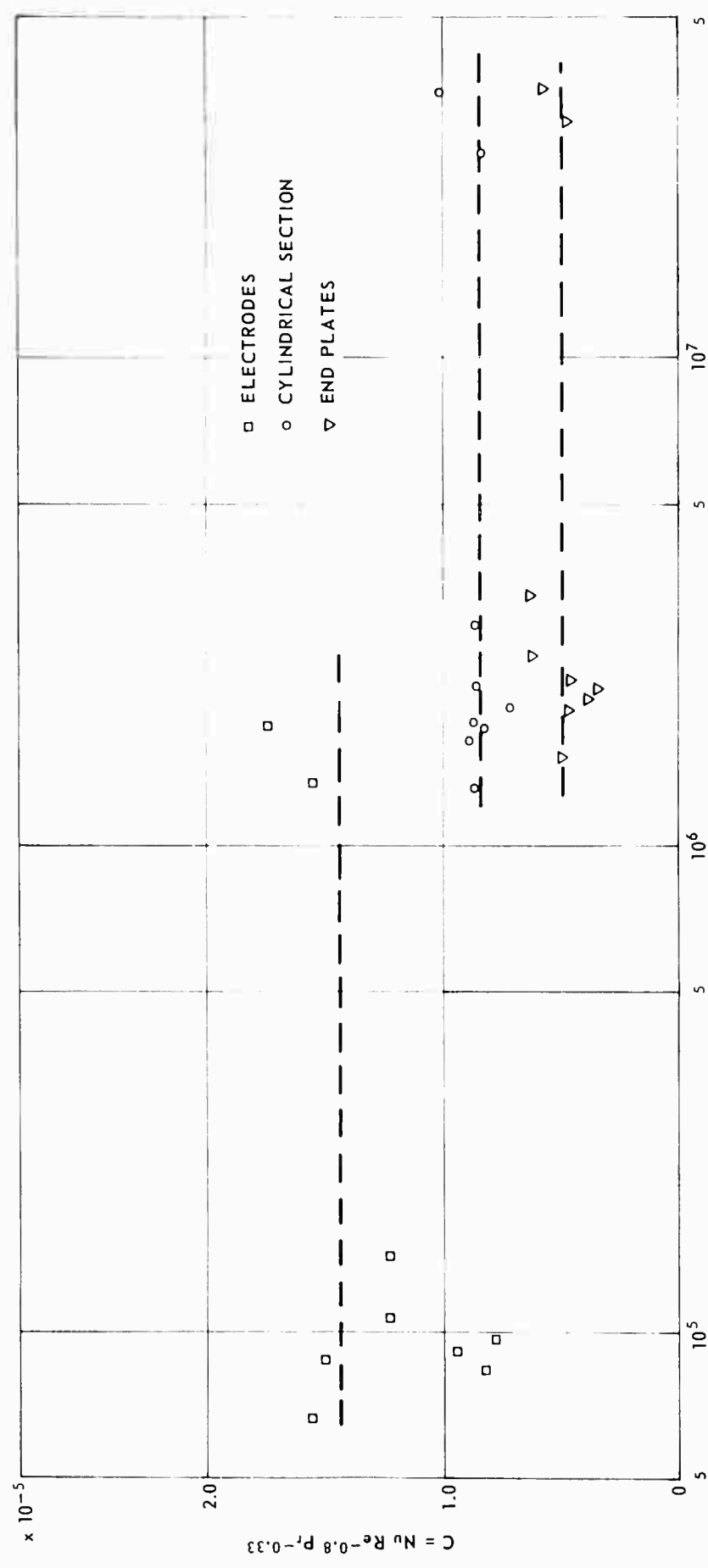


Fig. 11  $Nu Re^{-0.8} Pr^{-0.33}$  VERSUS  $Re$

## 6. CONCLUSIONS

While capable of further refinement, a satisfactory procedure has been developed for distinguishing radiative from convection losses in a split-ring type of plasma arc air heater; this in turn offers a means of optimization of efficiency. A satisfactory solution was obtained without taking arc radiation into account (the presence of which only affected the solution in the case of the electrodes). A value of gas emissivity was established that was nearly constant over the temperature range  $1600 < T < 6680^{\circ}\text{R}$  (the mean value of  $\epsilon/L$  being  $0.78 \text{ ft}^{-1}$ ) and that gave values for the most part much in excess of those given by tables for pure air. The excessive electrode losses were ascribed to the presence of arc radiation, which awaits a fuller theoretical treatment.

Convective losses were found to be proportional both to  $(\omega/\nu)^{0.8}$  and to the temperature difference with the walls (taken as the mean difference between gas and cooling water). However, although the correlation constant  $(\text{Nu} (\text{Re})^{-0.8} (\text{Pr})^{-0.33})$  was defined differently for the different surfaces, its value was unusually small--owing in all probability to the erroneous assumption that the forced vortex in the gas rotated at the same angular velocity as the arc, whereas it undoubtedly rotated more slowly. Notwithstanding this, two main conclusions were evident: (a) to keep convective losses low, the rotation rate should be limited to a value not exceeding  $150 \text{ sec}^{-1}$  by suitable choice of pressure, arc gap, and arc current, the effective limit of the last being about 15 kamps (for highest efficiency, it appears that a nonrotated arc

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would be best); (b) the relatively high emissivity of the copper-contaminated gas sets a practical limit on the enthalpy that may be achieved in an arc chamber of given volume and given input power. (For operation at similar power inputs but much higher enthalpies than those employed (e.g., 7000 Btu lbm<sup>-1</sup>) the chamber volume would need to be reduced to a much smaller value (e.g., 0.25 ft<sup>3</sup>).)



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\* A film illustrating split-ring arc rotation obtained at the Applied Physics Laboratory was contributed to this paper.

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13. ABSTRACT This paper is concerned with an analysis of the thermal behavior of high input power ( $\sim 15$  Megawatt) arc heaters operating at values of total (bulk) enthalpy up to 2500 Btu/lb. Such heaters are currently in use to supply air for aerodynamic testing purposes, including subsonic turbulent pipe flow, the operation of propulsion tunnels with "full" temperature simulation, and supersonic combustion ducts. The electrode system is essentially a "rail accelerator" adapted for continuous operation by making it re-entrant; the self-induced magnetic field brings about rapid movement of the arc roots to prevent destruction of the electrodes. The rate of rotation of the arc column (which is subject to aerodynamic drag) is shown to be a function of apparent electrode gap and current and the stagnation temperature and pressure in the arc chamber. A distinction can also be drawn between "long" and "short" arcs, depending on whether the interelectrode gap is large or small. The value of the arc rotation rate,  $\omega$  (which ranges between approximately 50 and 1000  $\text{sec}^{-1}$ ) had a considerable bearing on the thermal efficiency of short-gap arcs because of the dependence of the convective losses on it. Since the chamber gases radiated much more strongly than air uncontaminated by electrode material, convective and radiative losses are distinguished by solving for first-power and fourth-power dependence on temperature difference with the walls; the convective losses are examined in conjunction with a vortex model of the gas behavior.

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